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Isolation of hemicellulose from corn fiber

Abstract:

This invention pertains to a high yield process for producing high quality comfiber gum by hydrogen peroxide treatment of comfiber during alkaline extraction and/or after obtaining the alkaline extract of milled comfiber. This process comprises the steps: a) mixing comfiber with an alkaline solutionate form a slurry and extract hemicellulose; b) treating the slurry with hydrogen peroxide at a pH of about 10.0 to 12.5; and c) separating out the insoluble fractions from the comfiber slurry to yield comfiber gum. The comfiber gum produced by this process is highly soluble in water and provides low viscosity solutions which are nearly devoid of color over a wide pH range. The comfiber gum lacks objectionable flavor and aroma. The comfiber gum is useful for a variety of applications; including film formation and to thicken, emulsify, stabilize and/or extend aqueous solutions and suspensions.

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(57) Abstract

This invention permins to a high yield process for producing high quality coun fiber gum by hydrogen peroxide treatment of corn fiber during alkaline extraction and/or after obtaining the alkaline extract of milled corn fiber. This process comprises the steps: a) mixing corn fiber with an alkaline solution to form a sturry and extract hemicallulose; b) treating the shurry with hydrogen perturbed at apH of about 10.0 to 12.5; and c) separating out the insoluble fractions from the corn fiber alturny to yield corn fiber gum. The corn fiber gum produced by this process is highly soluble in water and provides low viscosity solutions which are nearly devoid of color over a wide pH range. The corn fiber gum lacks objectionable flavor and aroma. The corn fiber gum is useful for a variety of applications, including film formation and to thicken, emulsify, stabilize and/or extend equeous solutions and suspensions.

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ISOLATION OF HEMICELLULOSE FROM CORN FIBER

BACKGROUND OF THE INVENTION

1. Field of the Invention

Corn fiber is an abundant low-valued by-product of corn wet-and dry-milling industries, and for many years there has been an interest in developing more valuable products from it. The corn fiber gum (hemicellulose B) fraction is the most unique of the carbohydrate components of fiber and is potentially very useful. For corn fiber gum to attract significant commercial interest, however, it should be coloriess and lack the flavors and aromas normally associated with corn. This invention pertains to a process ifor the preparation of corn fiber gum which optimizes a yield of a white, highliquality product.

2. Description of Related Art.

valuable products from corn fiber. Hemicellulose is the major component of corn fiber (38-67%), followed by starch (10-30%), protein (15%), callulose (15%), oil (about 3.7%) and other substances such as lignin and asla (3%), (Osborn and Chen, (1984) <u>Starch/Staerks</u>, vol. 38, pp. 393-396; Carlson, T. (1994) In: <u>Proc. Corn Utilization Conference V. St. Louis, MO). Thenactual yields of corn fiber gum from corn fiber and brain, even on a dry and laterchfree basis, are quite variable and largely a function of the conditions used for its isolation.</u>

Early corn fiber gurn was prepared (Wolf, et al. (1953) <u>Cereal</u>

<u>Chemistry.</u> vol. 30, pp. 451-470) by boiling corn fiber for one hour at pH 10.5
11.6 followed by hot water extraction. Later efforts to lighten the color of corn fiber gurn resulted in extractions using sodium or calcium hydroxide, or

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combinations of the two, at various temperatures. Extracts using calcium hydroxide were the lightest in color and were further lightened by treatment with activated carbon. Yields in such cases were about 27%, and the hemicellulose A and B fractions were not separated. In addition, several processes for producing the arabinoxytan (hemicellulose B) fraction of fiber have been described in the patent literature, using various conditions of alkaline extraction (Wolf, supra; Rutenberg and Herbst, U.S. Pat. No. 2,801,955, 1957; Watson and Williams, U.S. Pat. No. 2,868,778; 1959; Schwelger, U.S. Pat. No. 3,716,526, 1973; Antrim and Harris, U.S. Pat. No. 4,038,481, 1977).

Later, Gould (U.S. Pat. No. 4,808,475, 1989) described a process for producing cellulosic products by treating nonwoody liignocellulosic agricultural byproducts with an aqueous solution of strong alkal and hydrogen peroxide. The lightin portion was thus solubilized, thereby enabling the separation of the non-soluble cellulosic portion from the soluble lightn portion. Chouset at. (U.S. Pat. No. 4,957,599, 1990) also described a process for delignifying and bleaching lignocallulosic material. The material was first treated with an atikatine solution free of peroxide, then an atikatine peroxide solution. Valid (U.S. Pat. No. 5,057,334, 1991) described the preparation of a callulose product by treating legume hulls with caustic alkaline oxidizing epent to solubilize the non-cellulose material, then dispersing the resulting wulp in water to form a slurry, lowering the pH of the slurry, then treating the slurry with aqueous hydrogen peroxide. In these efforts, peroxide served to toxidize lightn to low molecular weight organic acids, thereby altowing callulose to become accessible to the activity of cellulase. The objectives of these methods were to convert renewable lignocellulosic biomass to a form useful

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for glucose and ethanol production and for use at an energy source in ruminant feeds. To this end, success was achieved in minimizing loss of the hemicellulose fraction during alkaline peroxide extraction of plant sources.

Hemicelluloses are generally defined as polymers that are solutilized from plant cell walls by alkali (Darvill et al. 1980. Pages 91-140, in: The Biochemistry of Plants. P.K. Stumpf and E.E. Conn., eds. Academic Press, New York), and those from com fiber are typically corposed of D-xylose (48-54%), L-arabinose (33-35%), galactose (5-11%), anti D-glucuronic acid (3-6%) (Whistier and BeMiller (1956) J. Am. Chem. Soc. vol. 78, pp. 1163-№165; Sugawara, et al. (1994) Starch/Steerke. vol. 46, pp. \$35-337; Saulnier,:et al. (1995a) Carbohydr. Polym. vol. 26, pp. 279-287; \$aulnier, et al. (1995b) Carbohydr. Res. vol. 272, pp. 241-253). Most of the fraction is soluble in water after alkaline extraction. Their isolation is actually a two-stage process, involving alkaline hydrolysis of ester linkages to liberate them from the lignocellulosic matrix, followed by extraction into aquecus media. It is thus expected that com fiber gum is cross-linked to other cell wall components for several reasons. Both feruilic acid and p-cournaric abid are esterified to cell wall polysaccharides in various grasses (Muellel-Harvey et al. 1986. Carbohydr, Res. vol. 148, pp. 71-85). Partial acid (Yoshida, et al. (1990) Agric. Biol. Chem. vol. 54, pp. 1319-1321) and enzymatic (Ohta et al. (1994) J. Agric. Food Chem. vol. 42, pp. 653-656) hydrolysis of corn fiber gum yields oligosaccharide fragments in which arabinosyl units are esterified at primary hydroxyl groups with feruilc acid. Some were establised with diferuild acid (Saulinier, et al. supre) and acetyl esters were also identified on the erablnoxylan (Sauinier, et al. (1995a), supra). In addition, there is evidence to suggest that esterified feruilic and p-cournant acids serve to couple lignin and

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polysaccharide (Heim and Raiph (1993) <u>Carbohydr. Res.</u> vol. 240, pp.:23-38) and that polyphenolics (including lignin) can form alkali-resistant linkages with the hemicellulose fraction of the matrix polysaccharides (Morrison, I.M../1974) <u>Biochem J.</u> vol. 139, pp. 197-204; Fincher and Stone. (1986) pp. 207-295 In: <u>Adv. Cereal Sci. Technol.</u> VIII. Am. Assoc. Cereal Chem.: St. Paul, MN). Ether linkages are present in lignin, and there is evidence that ether linkages are also involved in linking lignin to hemicelluloses (Watanabe et al. /1989) <u>Agric. Biol. Chem.</u> vol. 53, pp. 2233-2252; Hatfield, R.D. (1991) Pages 285-313 In: <u>Forage Cell Wall Structure and Digestibility.</u> Jung et al., edst ASA-CSSA-SSSA: Madison, WI). As a result, most previous preparations of comfiber gum samples probably contained remnants of lignin, contributinglito off-colored products. Protein was also possibly present since stable linkages between hemicellulose and protein in com. bran (Baulnier, et al. (1995a), supra) and rye bran (Ebringerova, et al. (1994) <u>Cartohydr. Res.</u> vol. 284, pp. 97-109) have been identified.

Various optimization studies have been conducted to obtain useful high quality corn fiber gum in high yields. In preliminary experiments, corn fiber gum was isolated by standard extraction methods using salturated Ca(OH)₂ as extractant at 70°C for staten hours (Rutenberg and Merbat, supra) or under reflux conditions for one hour (Watson and Williams, supra). The 70°C extractions produced tarmish products. Yields ranged from 26.2 to 35.1% for extractions at 70°C and under reflux conditions, respectively.

At alkaline pHs, solutions of com fiber gum soluted by the traditional approaches turned intensely yellow, and the color doubt not be removed by dialysis. This was likely due to the presence of lighting or proteins which were retained even during extraction at elevated temperatures.

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Lighth fragments not removed from corn fiber gum with alkali were believed to contaminate corn fiber gum preparations, resulting the undesirable color. A method was developed for delignifying agricultural residues (Gould, J.M. (1984) <u>Blotechnol</u>, Bloand vol. 26, pp. 46152) to maximize their digestibility by ruminant animals. This method incorporated hydrogen peroxide in the extraction medium, which is capable of converting the lighth portion into soluble, low molecular weight organic acids. (It was shown (Gould, J.M. 1985b. <u>Blotechnol</u>, Bloang. vol. 27, pp. 225-23h) that delignification is most effective at about pH 11.5, the pK_a for the dissociation of hydrogen peroxide, and that the concentration of the species artive in delignification, "OH and *O₂, are optimal at pH 11.6.

Surprisingly, it has now been discovered that high quality corn fiber gum may be efficiently produced by hydrogen peroxide treatment of unmilled corn fiber during alkaline extraction and/or by hydrogen peroxide treatment after obtaining the alkaline extract of milled corn fiber.

SUMMARY OF THE INVENTION

This invention pertains to a high yield process for producing high quality corn fiber gum by hydrogen percode treatment of corn fiberiduring alkaline extraction and/or after obtaining the alkaline extract of milled corn fiber. This process comprises the steps:

- a) mbdng com fiber with an alkaline solution to form a slurry and extract hemiceliutose;
- b) treating the sturry with hydrogen percodde at a pH on about 10.0 to 12.5; and
- 25 c) separating out the insoluble fractibns from the com fiber sturry to yield com fiber gum.

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The com fiber gum produced by this process is highly solidible in water and provides low viscosity solutions which are nearly devoid or color over a wide pH range. The corn fiber gum lacks objectionable flavor and aroma. The corn fiber gum is usaful for a variety of applications, including film formation and to thicken, emulsity, stabilize and/or extend aqueous solutions and suspensions.

In accordance with this discovery, it is an object of the invertion to provide a process of preparing corn fiber gum by an alkaline hyperogen peroxide extraction process.

Another object of the present invention is to provide a novel cost fiber gum product prepared by an alkaline hydrogen percepte extraction process.

These and other objects of the present invention will become apparent to one skilled in the art from the following detailed description and examples below.

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BRIEF DESCRIPTION OF THE DRAWINGS

Fig. 1 shows one embodiment of the present alkaline hydrogen percede process of extracting corn starch.

Fig. 2A shows the effect of temperature on delignification of washed corn fiber at 25°C (•) and at 60° C (•), with an H_2O_2 to fiber ratio of 0.15.; 2B shows the effect of H_2O_2 to fiber ratios of 0.0625 (•) and 0.25 (•) on delignification of washed corn fiber at 60° C. Conditions: pH 11.5, liquid-to-fiber ratio, 15:1 (v/w).

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Fig. 3 shows the viscosity with temperature of corn fiber gum solutions (6 and 10% (wt/wt) solids) at pH 5.5; water at 5% (*), water at 10% (o), 100mM NaCl at 5% (*), 100mM NaCl at 10% (a), 100mM CaCl at 5% (*), and 100mM CaCl at 10% ().

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DETAILED DESCRIPTION OF THE INVENTION

This invention pertains to a high yield process for producing high quality corn fiber gum by hydrogen perceide treatment of corn fiber induring alkaline extraction and/or after obtaining the alkaline extract of milled corn fiber. This process comprises the steps:

- a) mixing com fiber with an alkaline solution to form a slurry and extract hemicaltulose;
- b) treating the slurry with hydrogen peroxide at a pH one about 19.0 to 12.5; and
- c) separating out the insoluble fractions from the corn fiber sturry to yield corn fiber gum.

Any base corn fiber may be used in the present application, including both those present in native corn and those present in corn produced by standard breeding techniques including cross-breeding, translocation, inversion, transformation or any other method of gens or chromissome engineering to include variations thereof. In addition, corn fiber present from corn grown from artificial mutations and variations of the above generic composition which may be produced by known standard methods of mutation breeding are also suitable herein.

Native come is intended to mean those varieties found in nature, including dent, waxy, or high armylose corn. As used herein, the term "waxy" is

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intended to include a starch or flour containing at least about 95% by weight armylopectin and the term "high armylose" is intended to include a starch or tour containing at least about 45% by weight armylose.

The corn fiber may be obtained during a wet-intiling or a dry-mixing process. The corn fiber may be dried and stored prior to use in the present extraction process, if desired.

Either ground or unground corn fiber samples may be utilized in the extraction process. The corn fiber is fragmented during the hydropen peroxide treatment, and the residues during and after treatment of both ground and unground fiber appear substantially the same. Apparently sufficient surface area is provided during the early stages of hydropen peroxide treatment to provide for efficient corn fiber gurn extraction. However, when no sikeline hydrogen peroxide stap is carried out prior to separation, and increase in yield typically occurs when using ground fiber of at least aboutil20 mesh rather than unground fiber.

There is no need to wash the corn fiber with either water or organic solvents prior to alkaline peroxide extraction though they may be washed.

Unwashed, unground corn fiber samples give comparable yields at a variety of extraction temperatures at pH 11.5 to washed corn fiber.

The com fiber is optionally destarched, particularly by inquefacation with oranglese until at least part, particularly substantially all, the starch-lie soluble. This may be carried out prior to alkeline extraction, or at any point in the process, including after the final com fiber gurn product has been obtained. Destarching prior to any filtration is generally preferred less otherwise the starch may clog the filtration equipment, particularly if the statch has been gelatinized.

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If destarched prior to the alkaline hydrogen peroxide treatment, the com fiber may be separated from the supermatant and rinsed with water to remove the soluble sugars and low molecular weight polysaccitarides produced by the starch hydrolysis. This results in a corn fiber gum which is more pure than that produced without removal of the starch hydrolysates.

Destarching may be done using any α -simplese and techniques known in the art. Other methods of destarching known in the art are also suitable, including separation of the starch from the fiber, i.e. by a hydrocyclone, or by use of other enzyme(s) or combinations thereof.

Any commercially available α -amylase is suitable for the present invention. The amount of enzyme is dependent upon the enzyme, i.e., source and activity, and base material used as well as the amount of hydrolysis desired. Typically, the enzyme is used in an amount of from about 0 to 20%, particularly from about 0 to 8%, more particularly from about 0.5 to 4% wwt/wt) of the corn fiber. For example, about 4.0% α -amylase (Termamyl commercially available from Novo Nordiak Bioindustrials, Inc.) has been found to be effective in the present invention.

Generally the enzyme treatment is carried out in an aqueous or buffered slurry at a corn fiber solids level of about 5 to about 40%. Alsolids level of from about 5 to 30% is particularly useful, from about 10 to 239 more particularly useful, in the instant invention.

The pH and temperature of the slurry should be adjusted to provide effective enzyme hydrolysis. These parameters are dependent upon the enzyme to be used and are known in the art. In general, a temperature of above about 75°C is suitable and the pH is adjusted to about 3.5 to about 8.5, particularly from about 4.5 to about 7.5, using techniques known in the art.

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The enzyme reaction is continued until the desired end point (i.e., sufficient degradation for the particular application) has been reached. The end point may be determined by a change in viscosity, by reducing sugar content, or by any other method known in the art for measuring the level of enzyme degradation of the starch molecule. In general, the enzyme reaction will take from about 0.1 to about 24 hours, particularly about 0.5 to about 4 hours. The time of the reaction is dependent upon the corn fiber and enzyme used, the amount of enzyme used, and the reaction parameters of solids percent, pH, and temperature.

The enzyme degradation may be terminated by any method known in the art, particularly acid deactivation or heat deactivation. However, termination of the degradation is not necessary.

Although destarching does not increase the yield or quality to the resulting corn fiber gum preparation, for uses where solution clarity and stability are required, fiber with a low starch content may be particularly suitable. When the starch content of the corn fiber is high, some residual starch may be found in the corn fiber gum extracts. Further, depending upon the separation technique(s) used, the presence of starch in the corn fiber may impede separation of the solids from the corn fiber gum.

The com fiber, whether or not destarched, is delignified by treatment with an alkaline hydrogen peroxide solution to extract hemicellulose from the fiber matrix. Further, treatment with an alkaline hydrogen peroxide solution may degrade colored impurities, resulting in a lighter colored corn fiber purp.

of the corn fiber is in the dry form, it is first slurred in water, particularly from about 10 to 20% solids. Sufficient water must be present to allow substantially uniform exposure to the alkaline hydrogen peroxide, but

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the addition of excess water may be detrimental to efficiency as more comfiber gum solution would need to be separated from the solids, and if sudned com fiber gum product was desired, more water would need to be evaporated.

The sturry is then basified by adding sodium hydroxide, potassium hydroxide, calcium hydroxide, and/or magnesium hydroxide in an amount necessary to bring the pH of the slurry to the range or from about 10.0 tol:12.5. To obtain greater yields, a pH of from about 11.2 to 11.8 is particularly suitable, more particularly from about 11.4 to 11.6, most particularly at about 11.5. In the alternative, the corn fiber may be slurried into such an alkaline solution.

However, higher pH tends to result in a final corn fiber gum product that is less white in color. Therefore, a slightly lower pH may be desirable for certain applications so that the yield is slightly lower than optimal, bat the color is lighter.

Hydrogen peroxide may be either added with the base or after the sturry has been basified. The hydrogen peroxide is ladded in an amount of from about 5 to 20% (w/wt) based on the corn fiber.

The temperature may then be raised, particularly to at least about 60°C, more particularly to about the boiling point for at least about half en hour, particularly for at least about one hour, though longer times may be used. In general, the time will be dependent upon the temperature of extraction, the pH, and the amount of hydrogen peroxible.

The amount of lighth degradation with all chillne peroxide may be monitored by any technique known in the art, such as the increase in obtical density at 260 nm. Lighth removal is generally maximized in about four isours

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at both about 25°C and at about 80°C, but about a 20% higher level of delignification products were produced at the higher temperatures (Fig. 2A). The effect of hydrogen peroxide level on delignification is shown in Fig. 2B. In general, increasing the ratio of hydrogen peroxide:fitter increases the level of delignification. The results of alkaline peroxide extractions of com fiber gum under different conditions are shown in Table I, Example 8.

The hemicellulose A is optionally separated from the corn fiber gum fraction. Hemicellulose A is the insoluble fraction of the hemicellulose while hemicellulose B (corn fiber gum) is the soluble fraction. However, hemicellulose A is soluble under alkaline conditions and is only insoluble under acidic conditions. The hemicellulose A therefore is typically responded by acidifying the corn fiber siurry to a pH of about 3.5 to 6.0, particularly from about 4.0 to 5.0. Any acid or combination, either mineral or organic, capable of lowering the sturry acidity to this range is suitable, particularly stilfuric, hydrochloric, phosphoric, acetic, or proplonic acid. Sulfuric acid is more particularly suitable as it generally produces a light colored corn fiber gum. Carbon dioxide gas is also suitable for acidification in the present process. The only limitation is that the acid used is acceptable for the ener use application.

The hemicellulose A yield by this process (on a dry, starch-free basis), generally is exceeded by that of the soluble corn fiber gum by/more than ten-fold. For example, extraction at 80°C results in a yield of hemicellulose A that is about 8% (w/wt) of that of corn fibers gum (hemicellulose B).

Hernicellulose A is water-insoluble. Determination of its removal depends upon the end use application. For example, if the application seeds

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complete solubility, such as in a beverage product, then it is important that hemicellulose A be removed using techniques known in the art, such has filtration. If the hemicellulose A is not removed, resulting solutions may be turbid or even may contain a precipitate, thus limiting the product usefulness. However, if the end use application does not require such stringent standards, the hemicellulose A does not need to be precipitated and separated from the corn fiber gum, for example in a cement mix or in certain cosmetic products. Further, if the end use application is alkaline in nature it is unnecessary to precipitate and separate the hemicellulose A from the corn fiber gum as it may remain soluble.

The solids are then separated from the solution containing the soluble corn fiber gum. The slurry may optionally be heated prior to separation to facilitate flow. The separation of the solids may be accomplished by a variety of techniques known in the art and is dependent upon the liquid:solid ratio, me particle size of the corn fiber, the presence or absence of starch, the pH and temperature of the aluny during separation, and the degree of purity desired. Further, more than one separation may be preferred, particularly from an efficiency standpoint. Typical separation processes include, but are not limited to filtration such as gravimetric, filter press, hor zontal plate, tubular, and vacuum filtration; centrifugation such as horizontal decenter and high speed disc centrifugation; microfiltration and ultrafiltration.

After separation of the solids, a second alkaline hydrogen peroxide treatment may be conducted. Such additional alkaline hydrogen peroxide treatment is carried out in the same manner as the first such treatment, but is generally carried out for a longer period of time, particularly at least about two

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hours. This second alkaline hydrogen perbxide treatment "further decomposes impurities and results in a lighter colored corn fiber gum.

If such second alkaline hydrogen peroxide treatment is carried out, the "solution" is typically separated a second time using any method known in the art, but generally one that will separate out undestrable fractions, such as salts, ash and other by-products of the hydrogen peroxide treatment. For example, the second separation may be accomplished by ultraffiltration or microfiltration. This second separation results in a purer product lead is particularly desired when the corn fiber gum is to be used for tood or pharmaceutical applications.

The pH of the slumy may be adjusted prior to any separation step. Generally, the pH is adjusted if necessary to prevent degradation of the comfiber gum and/or for safety reasons. The only situation in which the pHishould not be adjusted prior to the separation is when separation is used to remove any precipitated hemicellulose A from the slumy, as adjusting the pi-blout of the acidic range will allow the hemicellulose A to go leack into solution.

The resultant com fiber gum may be used directly in liquid form.

Alternatively, the com fiber gum may be recovered in powdered firm by conventional techniques known in the art, including drum drying, freeze titrying, and spray drying.

The comfiber gum may alternatively be precipitated from solution using lower alcohol extraction techniques. Lower alcohol is intended to mean a C₁₋₃ alcohol, particularly ethanol or isopropanol, more particularly ethanol. Alcohol precipitation of comfiber gum is known in the art and is particularly useful when a high degree of purity is desired, such as for pharmaceutical applications. Further, alcohol precipitation usually results in a lighter colored, purer product

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than many other separation techniques, le. spray drying, as less impurities remain in the product.

For example, about two volumes of ethanol are added to the corn fiber gum solution. The solution is then allowed to stand until the corn fiber gum settles out as a white floculant precipitate. The alcohol/water mixturexis then removed using techniques known in the art such as idecantation and filtration. The alcohol extraction may be repeated one or more times. The resulting corn fiber gum may then be dried, such as by air, oven, vacuum, fluid bed, freeze, or rotary drying. After the corn fiber gum is recovered, it may be ground to a smaller and/or more uniform particle size if desired using techniques known in the art.

The com fiber gum may also be modified using techniques known in the art such as crosslinking, derivatization, hydrolysis, and thermal inhibition. If desired, the corn fiber gum may be further purified using methods known in the art such as microfitration, ultralitration, reverse osmosis, bleaching/oxidizing, lon exchange, steam stripping, and carbon column fittation.

The purity and yield of the resultant com fiber gum will vary depending upon the process steps used and their order. In general, a yield of from about 25 to about 50%, particularly from about 35 to 50% (withwi) may be arbieved based upon the destarched com fiber.

The resultant corn fiber gum ranges in color from a very light lesign to white, depending primarity on the amount of purities which have been removed. It is highly soluble in water and provides low viscosity solutions which are nearly devoid of color over a wide pH range. The corn fiber gum lacks objectionable flavor and aroma. It is stable at least in the temperature range of 25 to 60°C in both water and in salt solutions (solitum or calcium chioride).

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The resultant corn fiber gum also has excellent water holding capabilities.

Such property is desirable for numerous applications including adhesives and cement. It is also stable over a wide pH range.

The resultant corn fiber gum is useful in the same applications as previously known corn fiber gums, including for film formation and to thicken, emulsity, stabilize and/or extend aqueous solutions and suspensions. Specifically, corn fiber gum is useful in food products, pharmaceinticals, cosmetics and personal health products, cement, and adhesives. This com fiber gum may also be used as a rheological mobilier such as in reality, coatings, and films.

The general process, above, for producing com fiber gum may be done using several alternative orders, each producing different yields and/or purities of com fiber gum. For example, the com fiber may be basified, the solids may be separated out, and then the aliquine hydrogen peroxide treatment may be carried out. The critical element of the process is carrying out the hydrogen peroxide treatment at alkaline pH. In general, the remainder of the steps can be carried out by those of skill in the art by following routine procedures or the description contained herein. Determination of the process steps and conditions to be used is dependent upon the desired properties of the com fiber gum.

The following examples are intended only to further illustrate the invention and are not intended to limit the scope of the invention as defined by the claims.

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EXAMPLES

Example 1 - Process of Extracting Com Fiber Gum

Destarching

- a. Com fiber (3500g anhydrous) was added to 70 liters of water and mixed well. The pH was adjusted to 7.0 with 25% NaOH. The slurry was heated to 85°C and the pH was readjusted to 7.0. 140g of Termamyl 120 L (commercially available from Novo Nordisk Biolindustrials, inc., Danbury, CT). The temperature was held at 85°C with mbdng for four hours. The lielumy was cooled to room temperature and dewatered using a perforated bowl centrifuge. The corn fiber was washed with water two times on the bowl
 - b. The destarching of Example 1a was repeated and the corn fiber was dried after being washed.

Alkeline Hydrogen Peroxide Treatment

The destarched corn fiber (3000g anhydrous) was added to 60 liters of water with mixing. 240g of sodium hydroxide pellists and 222g of chickum hydroxide were added to the mixture, 1000g of hydrogen peroxide (30% solution) was then slowly added. The mixture was heated to 95°C and held for one hour with mixing. The mixture was acidified to pH 4.5 with: 25% sulfuric acid and cooled to room temperature.

Separation

a. The insoluble meterial was separated unting a Sharples *P-860 horizontal decanter centrifuge, followed by a BTFX 205 high speek disk centrifuge (both commercially available from Alfa Laval, Inc., Warminster, PA).

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b. The Insoluble material was separated out as in Example 1a separation and the centrate was further clarified using an ultrafiltration membrane with 300,000 molecular weight cutoff.

Isolation

- The centrate was concentrated to between 10 and 15% solids, if necessary, and then spray dried using an Ahydro Lab #1 spray drier (commercially available from Anhydro Lab, Attleboro Falls MA) with an intert temperature of 250°C and an outlet temperature of 85-95°C. The pH was kept in the range of 5 to 9.
- b. Two volumes of 95% ethanol were added to rapidly attred centrate. After allowing the corn fiber gum to settle out as a white flocculant predipitate (about 10 min), the alcohol/water mixture was removed by decentation. The precipitate was removed by filtration, air-dried in a fume hood and then in vacuum over at 50°C for one hour. The resultant own fiber gum was a fine white powder.

Example 2 - Process of Extracting Com Fiber Gurn Using a Second Attaline : Hydrogen Peroxide Treatment

Destarching

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The corn fiber was destarched using the destarching procedure of Example 1.

Alkaline Hydrogen Peroxide Treatment

The corn fiber was treated with alkaline hydrogen peroxide using the alkaline hydrogen peroxide procedure of Example 1.

25 Separation

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The insoluble material was separated using the separation producture of Example 1.

Second Alkaline Hydrogen Peroxide Treatment

1000g of hydrogen peroxide (30% solution) were added to the centrate obtained from the solid-liquid separation. The pH of the mixture was adjusted to 11.5 with 25% sodium hydroxide and agitated for two hours. The mixture was neutralized to pH 7.0 with 25% sulfuric acid and then ultrafiltrated to further clarify the centrate.

legiation

10 Corn fiber gum was isolated using the isolation procedure of Example 1.

Example 3 - Process of Extracting Corn Fiber Gum Using Alkaline Hydrogen Perceide Treatment After Separation

15 <u>Destarching</u>

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The corn fiber was destarched using the distarching procedure of Example 1.

Alkaline Extraction

The destarched corn fiber (3000g anhydrous) was added to 60 liters of water with mixing. 240g of sodium hydroxide pellists and 222g of calcium hydroxide were added to the mixture. The mixture was heated to 95% and held for one hour with mixing. The mixture was additied to pH 4.5 with 25% sulfuric acid and cooled to room temperature.

Separation

The insoluble meterial was separated using the separation procedure of Example 1.

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Alkaline Hydrogen Peroxide Treatment

1000g of hydrogen peroxide (30% solution) were added to the centrate obtained from the above solid-liquid separation. The pH offlithe mixture was adjusted to 11.5 with 25% sodium hydroxide and agitated for hours. The mbdure was neutralized to pH 7.0 with 25% sulfuric acid.

Second Separation

- The mixture was ultrafiltrated to further clarify the centrate using the separation procedure of Example 1b.
- No separation was done.

10 Isolation

The corn fiber gum was isolated using the solation procedure of Example 1.

Example 4 - Process of Extracting Corn Fiber Glim Using a Second

15 Separation Step

Destarching

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The corn fiber was destarched using the destarching procedure of Example 1.

Alkaline Extraction

The destarched corn fiber (3000g anhydrous) was added to 60 liters of water with mixing, 240g of sodium hydroxide pellets and 222g of calcium hydroxide were added to the mixture. The mixture was heated to 95°C and held for one hour with mixing. The mixture was cooled to room temperature.

Separation

The insoluble mixture was separated using the separation procedure of Example 1a.

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Alkaline Hydrogen Peroxide Treatment

1000g of hydrogen peroxide (30% solution) were added no the centrate obtained from the above solid-liquid separation. The pH of the mixture was adjusted to 11.5 with 25% sodium hydroxide and agitated for two hours. The sturry was then acidified to a pH 4.5 with 25% sulfuric acid.:

Separation

The insoluble material is separated out using the separation procedure of Example 1b.

<u>Isolation</u>

The com fiber gum is recovered using the isolation procedure of Example 1.

Example 5 - Process of Extracting Corn Fiber Gum Using Carbon Dioxide to Acidity

15 Destarching

The corn fiber is destarched using the destarching procedure of Example 1.

Alkaline Hydrogen Peroxide Treatment

- a. The destarched corn fiber (3000g anhydrous) was added to 60 litters
 of water with mixing, 240g of sodium hydroxide petiats and 222g of chicium
 hydroxide were added to the mbdure, 1000g of hydrogen perceide#(30%
 solution) were then slowly added. The mbdure was nested to 85°C and held
 for one hour with mixing. The mbdure was addified to pH 4.5 with carbon
 dioxide gas and cooled to room temperature.
- 25 b. The procedure of 5a was followed, except that dry ice is used as the source of carbon dioxide.

Secaration

The insoluble material was separated using the separation procedure of Example 1.

30 <u>lactation</u>

The corn fiber gum was isolated using the isolation procedure of Example 1.

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Example 6 - Comparison of Yields Using the Various Processes of Extracting Com Fiber Gum

The percent (wt/wt) yield of corn fiber gum resulting from the above processes were determined based on the destarched corn fiber.

<u>Samole</u>

Percent Yield (wir/wt)

Example 1

42.7

Example 3

32.7

Example 7 - Variation on Process of Extracting dom Fiber Gum Using a Second Separation Step

Destarching

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Com fiber samples were ground to a particle size of 20 mesh using a Wiley mill. Moisture levels were determined after drying the samples to a constant weight in a vacuum oven at 80°C. Stards was removed from the ground fiber by sedimentation followed by treatment with the α-anaylase, Termamyl (commercially available from Novo Nordisk Bioindustrials: Inc., Danbury, CT). Com fiber (770 g, 20 mesh) was stirred in a cylinder with seven liters water and the mbiture was then allowed to settle. The starch granules were concentrated in the upper portion of the sediment, and they were removed by decantation. After repeating this process four times, the fiber/water sediment was diluted to five liters with water. This mixture was attirred at 95°C for two hours at pH 6.5 with 50 m α-amylase, in order to liquefy residual starch. The residue was collected by filtration, washed with distilled, delonized water (five liters) in order to remove any remaining maltodexirths, and dried in a vacuum oven at 50°C.

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Alkaline Extraction

- a. Ground com fiber (100 g) was mechanically stirred at 85-90°C into one liter of water. Sodium hydroxide (8 g) were added so that a total of 2 may alkalig fiber were present in the extraction medium. The mixture was boiled with mechanical stirring for one hour.
- b. Example 7s was repeated using 7.4 grams calcium hydroxide in place of the sodium hydroxide.

Separation

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Residue was removed by centrifugation (6,000 x g for about 10 min), and the corn fiber gum-containing supernatant was removed by decastation (about 660 mi). The remaining fluid (about 340 mi) remained associated with residue and contained about one-third of the extracted hemicellusose. Additional corn fiber gum was recovered by adding 800 ml water to the residue and boiling the mixture for five minutes with stirring. This mixture was then centrifuged and the supernatant combined with that of the original extract. The total volume of extracts was about 1.4 liters. This procedure was repeated in order to isolate additional corn fiber gum.

Alkalina Hydrogen Peroxide Treatment

To the extract of 100 g fiber was added 10 g hydrogen peroxidel(33.3 m) of 30% $\rm H_2O_2$). After adjusting the pH to 11.5 by addition of 50% NaCH, the solution was stirred at ambient temperature for two hours.

Separation

a. The H₂O₂-treated atkaline extract was adjusted to pH 4 to 4.5 by addition of HCI (concentrated, about 37%). After 15 minutes, the hemicellulose A precipitate was removed by vacuum filtration throught Celite filter aid.

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b. The above separation was repeated using centrifugation at 10,000hx g for 10 minutes.

solution

Two volumes of 95% ethanol were gradually added to the stirate. After allowing the corn fiber gurn to settle out as a white flocculant precipitate (about 10 min), the alcohol/water mbdure was removed by decentation. The precipitate was stirred in 95% ethanol for five minutes, removed by filtration, air-dried in a fume hood and then in vacuum over at 50°C for one hour. The corn fiber gurn recovered was then converted to a line white powdertwith a conventional chopper-grinder.

Example 8 - Comparison of Hamicallulose Yields Extracted Under Different Conditions

Com fiber (3.0 g; 20 mesh destarched, unground not destarched) and aqueous 30% hydrogen peroxide (2.5 ml) were added to rapidly stirrediserter (75 ml, deionized and distilled), to give a 0.25 ratio of hydrogen peroxide to fiber, and a 1% aqueous solution of H₂O₂. The pH was adjusted to 1%,5 by addition of 2N NaOH (9 ml). Under these conditions, there were about 15 meq NaOH per gram of fiber. Reactions at 25°C were conducted in Erlenmeyer flasks on magnetic stirrars, while those at 60°C were conducted in a jacketed reaction vessel heated with water from a thermostat-controlled circulating bath. During initial stages of stirring, oxygen evolution was active, and substantial frothing occurred, requiring that extractions be conducted in vessels with volumes two to three times those of extraction mixtures. The pH during extractions were maintained at 11.4 to 11.6 by dropwise addition of 50% NaOH. After removing residue by centrifugation at 3,000 x g for 16 min,

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the supernatant fluid was adjusted to pH 4.0 with 4N HC (about 2 mi). The hemicallulose A fraction was allowed to precipitate overnight, and then collected after centrifugation at 10,000 x g for 10 min. The supernatant fluid containing corn fiber gum was removed by decantation. The hemicallulose A precipitate was washed with isopropanol, collected by filtration, and then dried in a vacuum oven at 50°C. Corn fiber gum was precipitated by pouring the supernatant fluid into two volumes of stirred isopropanol, from which it settled out as a white flocculant precipitate. Corn fiber gum was collected after carefully decanting off the supernatant fluid. It was transferred with the aid of isopropanol to a beaker, and the moture was stirred for 5 min. This converted the material from a sticky and rubbery state to a more workable form. Next the corn fiber gum fraction was collected (filtration, centrifugation), or sieve), and air-dried in a furne hood for one hour, finely fragmented with a conventional chopper-grinder, and dried to constant weight in a vacuum oven at 50°C.

The yields of the com fiber gum are shown in Table 1, below.

Table I

Yields of Hamicellulose A and B from Alkaline H₂O₂ Extraction of Com Fiber

20	REACTION CONDITIONS HEMICELLULOSE YIELD, %°					
	Trial	Com Fiber B A	initial pH	Temp., °C	Time, hr	
25	_		44.5	0.5	i a	
	A	20 Mesh 15 3.1	11.5	25	8	
	В	20 Mesh 35 3.5	11.5	26	24	
30	C	20 Mash 36	11.5	25	72	
	D	20 Mesh 41 2.8	11.5	60	2	
	E	20 Mesh	12.0	25	8	
35		35 4,2			[
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	F	20 Mes h 40 3.7	12.0	25	24	
	G	20 Mesh 32 8.3	12.0	60	2	
5	н	20 Mes h 51 4.2	11.5-12.5°	80	2	
	1	Unground 35 0.4	11.5	25	24	1
10	J	Unground 38	11.5	25	72	
	K	Unground 42 1.7	11.5	60	2	1
	L	Unground 47 8.5	11,5-12,5°	60	2	•
15	M	Unground 46 4.2	11.5-12.5°	26	24	

Extractions were conducted using fiber-alkaline solution-H₂O₂ ratios of 1:25:0.25 (w/v/w); 20 mesh fiber samples were destarched, and the unground fiber samples were unwashed.

Application of the alkaline hydrogen peroxide process to 204mesh fiber at 25°C indicated a doubling of corn fiber gurn yield between an 8 and 24 hour (rows A.B) extraction period. An extraction in which the proportion of hydrogen percodde to fiber was increased from 0.25 to 0.50 resulted in an increase in the yield of com fiber gum after 72 hours at 25°C from 36% (row C) to 46%. The corn fiber gum was nearly white, and the recovered residue was off-white. In 8 hours, 25°C extractions, the yield more than doubled when the pH was increased from 11.5 to 12.0 (rows A,E). In 24 hours at 25°C, only a modest gain in yield was achieved by increasing the pili from 11.5 to 12.0 (rows B,F). At 60°C, a higher yield of com fiber gum was obtained at pH 11.5 than at pH 12.0 (rows D,G). This is the trend that would be expected, since pH 11.5 is the optimal pH for lignth oxidation. At 60% and pH 12.0, 26% of the corn fiber gum was hamicallulose A (row G). A maximum com fiber gum yield of 51% was obtained at 60°C by processing at

^b Yields for all trials are reported on a dry, starch-free basis.

c Initial pH of 11.5 was increased to 12.5 after half extraction time had eleosed.

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pH 11.5 for the first hour and then increasing the pH to 12.5 for the final hour (row H). When using unground corn fiber, as with 20-mesh fiber, little sain in yield resulted from extending the 25°C process beyond 24 hours (rows I,J). By comparing results using ground and unground fiber, it is clear that the energy intensive grinding step provides little advantage in terms of corn fiber gum yield (rows B,I, C,J, D,K, F,M, and H,L).

Corn fiber gum yields were reduced by more than one-third when extractions were conducted in the absence of hydrogen peroxide. Using conditions such as Trial D (Table I), for example, the yield dropped from 41 to 25%. When color as well as yield is considered, the process is most effective when conducted at pH 11.5. Possibly at the elevated pH, especially at 80°C, chromophores are generated by sikeli-catalyzed modification of reducing end groups on the polysaccharide. The corn fiber gums generated at pH 11.5 were off-white, while those exposed to pH values of 12.0 and 12.5 were teamlish, even when the extractions were done at room temperature. A two hour reaction period at pH 11.5 and 60°C with unground fiber (row K) gave a 42% yield of off-white corn fiber gum, with a very low level (1.7%) of hemicellulose A. Kernel pericarp, when extracted under these conditions, yielded off-white corn fiber gum in a 24% yield.

The results in Table I were from experiments using solutions with a ratio of fiber to alkall to hydrogen percede of 1:25:0.25. Under these conditions, most of the fluid (and com fiber gum) was isolated after remeval of residue by centrifugation. When solutions with higher ratios of fiber to alkali were used, however, significant quantities of fluid and associated com fiber gum remain with the swelled residue. Then it is necessary to redispense the residue in additional water to extract residual com fiber gum. When

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extractions are conducted at fiber to liquid ratios of \$1.10, substantial amounts of corn fiber gum-containing fluid remained associated with the residues since it became very swellen and absorbent. Only about 70% of the fluid is isolated after the initial centrifugation and decantation, so as much as 30% of product could remain in the fluid associated with the residue.

When the isolated corn fiber gum preparations were taken up in alkaline peroxide at pH 11.5, no additional 280 nm absorbing material was generated, indicating that all lightn susceptible to degradation had been removed.

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Example 9 - Compositions and Properties of Com Fiber Gum Extractes Using Different Alkatine Solutions

Corn fiber was ground to a 20 mesh using a Wiley mill. 500 grof the corn fiber were stirred in four liters water and the pill was adjusted to 6.5 by addition of a 50% solution of sodium hydroxide at 85-90°C. 20 ml α -amylase (Termamyl) were added and allowed to treat for four hours. The corn fiber was then separated out by centrifugation and decantation. The fiber was washed with water, then ethanol and dried in a 60°C oven.

100g of the destarched com fiber was stirred into one liter water and 2 med alkalify fiber were added (NaOH; Ca(OH)₂; or 1:1 (equimolar) mixture). The mixture was boiled for one hour. The residue was removed by contrifugation and the supernatant was removed by decantation. 800m* water were added to the residue and the mixture was boiled for five minutes with mixing. The mixture was then centrifuged and the centrate was combined with the supernatant to produce 1.4 liters.

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10g hydrogen peroxide (33.3 ml of aqueous 30% hydrogen peroxide) were added with stirring, the pH was adjusted to 11.5 by addition of 50% sodium hydroxide, and the reaction was allowed to propeed for two hours.

The treated extract was adjusted to pH of 4.0 to 4.5 by addition of concentrated hydrochloric acid. After 15 to 30 minutes, the hemicalluidea A precipitate was removed by filtration through Celite. Two volumes of \$95% ethanol was stirred into the filtrate and the corn fiber gum was allowed to settle out as a white flooculant precipitate (10 minutes). Corn fiber gumbwas collected after carefully decanting off the supernature fluid. The precipitate was stirred in 95% ethanol for five minutes, isolated by filtration, air driedliand then dried in a vacuum oven at 50°C for one hour. The corn fiber gum product was finely fragmented with a conventional chapper-grinder, and stried to constant weight in a vacuum oven at 50°C. The resulting corn fiber gum was analyzed using methods known in the art and the percent yield (wit/wt) was determined based on the destarched corn fiber. The results are shown in Table II, below.

TABLE II

	NaOH only	NaOH:Ca(OH)₂ = *:1	Ca(OH)₂ only
percent yield*	40	27	21
esh (%)	2.15	2.42	2.6 .
N (%)	0.151	D.1B3	0.126
Ca (%)	0.30	0.63	0.56
MW (Kda) ^b	3.94 (0.04)	B.03(0.10)	2.78(0.05)
WI ^e	38.9	49.4	50.0
Arabinose ^d	39.4	40.6	37.
Xytose ^d	48.1	49.6	49.f.

-29-

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